

Fluid Simulation on Cartesian Grid

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Background of Research Application of CFD

> Complex Geometries Moving Boundary

Difficultly of Grid Generation

Purpose of Research

Development of

- 1. Automatic Grid Generator
- 2. Numerical Method



Research Areas

Cut Cell Method AMR(Adaptive Mesh Refinement) Cartesian/Structure Hybrid Method Locally Body-Fitted Cartesian Grid

Image of Cartesian Grid



Simple Cartesian Grids



Cut Cell with Cell Merging





LMR(Local Mesh Refinement



Locally Body-Fitted Cartesian Grid



Diagonal Cartesian Grid



Numerical Algorithm

Computational Method

Finite Volume Method (FVM)Fractional Step MethodCollocate Grid Method

Governing Equations

Navier-Stokes Eq.

$$\frac{\partial u_i}{\partial t} + \frac{\partial u_j u_i}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \frac{1}{\operatorname{Re}} \frac{\partial}{\partial x_j} (\frac{\partial u_i}{\partial x_j})$$

Continuity Eq.

$$\frac{\partial u_i}{\partial x_i} = 0$$

Fractional Step Method

$$\frac{u^* - u^n}{\Delta t} + \frac{1}{2} (3N_u^n - N_u^{n-1}) = \frac{1}{2 \operatorname{Re}} \nabla^2 (u^* + u^n)$$
$$\frac{v^* - v^n}{\Delta t} + \frac{1}{2} (3N_v^n - N_v^{n-1}) = \frac{1}{2 \operatorname{Re}} \nabla^2 (v^* + v^n)$$

Poisson Eq. For Scalar ϕ

 $\nabla^2 \phi = \frac{\nabla \cdot V^*}{\mathbf{A}}$

Correction of velocity and pressure

$$u_i^{n+1} = u_i^* - \Delta t \frac{\partial \phi}{\partial x_i}$$

$$p = \phi - \frac{\Delta t}{2\text{Re}} \nabla^2 \phi = \phi - \frac{1}{2\text{Re}} \nabla \cdot V^*$$

Collocate Grid





Cut Cell Based Cartesian Grid

Cut Cell with Cell Merging



Cut Cell With Merging Treatment

Point of Cut Cell

The value and gradient of ϕ must be expressed at cut faces.



Cut Cell without Merging Treatment P,V Ρ The value and gradient of ϕ must be expressed at cut faces.



Driven Cavity Flow



Numerical resutls



Flow around a circular cylinder

30D



Uniform flow

Sommefeld Reflection BC

Results (Re=200)

	C _D	C _L	St
Cut Cell	1.36 ± 0.04	± 0.67	0.20
Body Fitted Grid	1.34 ± 0.04	± 0.65	0.19
Roger et al. (1988)	1.29 ± 0.05	± 0.75	0.16
Rosenfield et al. (1991)	1.31 ± 0.04	± 0.65	0.20
Rosko (1954) exp.			0.19
Wille (1960) exp.	1.30		

Results(Re=1000)

	C _D	C _L	St
Present Method	1.51 ± 0.22	± 1.40	0.23
Cell Merging Method	1.65 ± 0.22	± 1.45	0.26
Body Fitted Grid	1.50 ± 0.20	± 1.37	0.25
Mittal et al. (1997)	1.53 ± 0.24	± 1.37	0.245

3D Finite Length Cylinder



3D Finite Length Cylinder

time=1

Cut Cell with Moving Boundary



Comparison with Exact solution



Numerical Grids

Comparison of flow rate

Flow around oscillating cylinder

Time histories of CD and CL

BFC with ALE



Comparison of CD and CL

	C _D	C _L	St
BFC	1.61 ± 0.22	± 0.71	0.20
CutCell	1.60 ± 0.23	± 0.69	0.20

Rotating Square Cylinder Re=1370



Comparison with Exp. results



Re=1370, ω=0.628)

Flow in a 2D Mixer







Flow around a F1



LMR and AMR Techniques

Flows in Driven Cavity



AMR for a Cylinder



AMR on Track



AMR on a Track



AMR on a Car



AMR on Car







Cartesian/Structure Hybrid

Cartesian/Structured Hybrid Grid



LBFCGM (Locally Boundary Fitted Cartesian Grid Method)



BFC generating based Cut Cell





LBFCGM for Thin Body



Treatment at connect cells



Numerical Results at Re=200

	C _D	C _L	St
Present Method	1.34 ± 0.04	± 0.62	0.21
Cell Merging Method	1.31 ± 0.05	± 0.66	0.20
Body Fitted Grid	1.34 ± 0.04	± 0.65	0.19
Roger et al. (1988)	1.29 ± 0.05	± 0.75	0.16
Rosenfield et al. (1991)	1.31 ± 0.04	± 0.65	0.20
Rosko (1954) exp.			0.19
Wille (1960) exp.	1.30		

Early Stage of the Wake



Re=40(T=12)



L/D Re=40



a/D, b/D Re=40



Re=3000(T=2.5)



L/D Re=3000



a/D,b/D Re=3000



Flow around Two-Cylinders

30D



CD and CL (Re=100, S/D=2.5)



CD and CL (Re=100, S/D=5.5)



Comparison of results (Re=100)

S/D			First cylinder	Second cylinder
		CD	1.230 ± 0.001	-0.098 ± 0.001
	Present	CL	0.000 ± 0.001	0.000 ± 0.003
2.5		St		
	S. Mittal et	CD	1.271 ± 0.0	-0.075 ± 0.0
	al. (1997)	CL	0.000 ± 0.0	0.000 ± 0.0
		St		
5.5	Present	CD	1.334 ± 0.014	0.849 ± 0.150
		CL	0.000 ± 0.404	0.000 ± 1.621
		St	0.165	0.165
	S. Mittal et	CD	1.433 ± 0.015	0.952 ± 0.164
	al. (1997)	CL	0.000 ± 0403	0.000 ± 1.741
		St	0.168	0.168

2D Inlet Flow of a Fluidic Flow Meter


The Vectors



3D Inlet Flow of a Fluidic Flow Meter



Inlet Flow of a Fluidic Flow Meter With Complex Geometry



Tube banks with tandem arrangement



Tube banks with tandem arrangement



Tube banks with staggered arrangement



Tube banks with staggered arrangement



Moving Boundary Problem



Moving Boundary Problems



Thank You!